

## Hot corrosion behavior of $\text{Ti}_3\text{SiC}_2$ in the mixture of $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$ melts

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### Abstract

The corrosion behavior of polycrystalline  $\text{Ti}_3\text{SiC}_2$  was studied in the mixture of  $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$  melts with various mass ratios at 850 °C. The results demonstrated that  $\text{Ti}_3\text{SiC}_2$  suffered from serious hot corrosion attack in the mixture of  $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$  melts when the concentration of  $\text{Na}_2\text{SO}_4$  was higher than 35 wt.%. A large amount of corrosion products spalled from specimens during the tests and obvious mass loss was observed. Hot corrosion of  $\text{Ti}_3\text{SiC}_2$  would become severe because  $\text{NaCl}$  had lower melting-point and caused  $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$  mixture melted below 850 °C. However, when the concentration of  $\text{Na}_2\text{SO}_4$  was lower than 25 wt.% in the mixture, a protective oxide layer ( $\text{SiO}_2 + \text{TiO}_2$ ) formed on the substrate, the corrosion rate of  $\text{Ti}_3\text{SiC}_2$  became quite slow and slight mass gain was observed, the corrosion products did not spall from substrate at 850 °C. The microstructure and phase composition of the corroded samples were investigated by SEM/EDS and XRD. © 2004 Elsevier Ltd. All rights reserved.

**Keywords:**  $\text{Ti}_3\text{SiC}_2$ ; Corrosion; Molten salts; Hot corrosion;  $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$  melts

### 1. Introduction

Ceramics are generally thought to possess many of the properties desired for higher-temperature replacements of superalloy: high melting points, high-temperature strength, low density, and increased resistance to aggressive environments. The primary shortcoming of monolithic ceramics is their lack of acceptable low-temperature ductility and toughness.  $\text{Ti}_3\text{SiC}_2$  with a layered crystal structure possesses a combination of the properties of both metals and ceramics. The theoretical density is 4.53 g cm<sup>-3</sup>.<sup>1</sup> It has a hardness of 4 GPa, a Young's modulus of 325 GPa, a room temperature fracture toughness about 7 MPa m<sup>1/2</sup> and quite damage tolerant. It exhibits a brittle-to-plastic transition around 1100 °C; at 1300 °C, the material is plastic with 'yield' point of 100 and 500 MPa in flexure and compression, respectively. At room temperature, it has electrical and thermal conductivities of  $4.5 \times 10^6 \Omega^{-1} \text{m}^{-1}$  and 37 W m<sup>-1</sup> K<sup>-1</sup>, respectively.<sup>1–6</sup> These unusual combinations

of the properties render it a candidate structural material for high-temperature applications. When it was oxidized in air, a protective oxide scale formed in layers, where the inner layer was composed of a mixture of  $\text{SiO}_2$  and  $\text{TiO}_2$  and the outer layer was pure  $\text{TiO}_2$ . Oxidation kinetics follows a parabolic law in the 900–1300 °C temperature range with an activation energy of about 370 kJ mol<sup>-1</sup>.<sup>7</sup>

Industry systems are such as heat engines and heat exchangers involve harsh environments. The structural materials are subjected to high temperatures, corrosive gases and condensed phases such as  $\text{NaCl}$  and  $\text{Na}_2\text{SO}_4$ . Under the appropriate conditions these salts deposit on substrate, which lead to severe hot corrosion attack and accelerated degradation of materials.<sup>8</sup> From the point of view of application, to evaluate corrosion resistance of a material is important in corrosive environments. Liu et al.<sup>9–11</sup> studied the hot corrosion behavior of polycrystalline  $\text{Ti}_3\text{SiC}_2$  induced by molten  $\text{Na}_2\text{SO}_4$  and  $\text{Li}_2\text{CO}_3$ – $\text{K}_2\text{CO}_3$ , respectively. The results demonstrated that  $\text{Ti}_3\text{SiC}_2$  ceramics coated with about 2 mg cm<sup>-2</sup>  $\text{Na}_2\text{SO}_4$  suffered from serious hot corrosion at 900 and 1000 °C.<sup>11</sup> When  $\text{Ti}_3\text{SiC}_2$  was immersed in  $\text{K}_2\text{CO}_3$ – $\text{Li}_2\text{CO}_3$  eutectic mixture in the 700–850 °C temperature range, obvious mass loss was ob-

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served, severe hot corrosion occurred and led to strength degradation.<sup>9,10</sup> However, up to now, investigations focused on the corrosion behaviors of  $\text{Ti}_3\text{SiC}_2$  in the mixed salts of  $\text{Na}_2\text{SO}_4 + \text{NaCl}$  were seldom reported. The aim of this work is to report the hot corrosion behaviors of  $\text{Ti}_3\text{SiC}_2$  in the mixture of  $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$  melts. The results are useful for selecting the appropriate conditions for the application of this technologically important material.

## 2. Experimental

### 2.1. Specimen preparation

$\text{Ti}_3\text{SiC}_2$  used in this work was TSC<sup>ZS510</sup>, which was fabricated by the in situ hot pressing/solid–liquid reaction process, which was described elsewhere.<sup>12</sup> The  $\text{Ti}_3\text{SiC}_2$  content was determined to be 93 wt.% by the Rietveld method in Cerius<sup>2</sup> computational program for material research (MSI, USA) using DBWS code and the major impurity was TiC. The density of the materials is  $4.52 \text{ g cm}^{-3}$ , and the porosity is less than 1%. Rectangular specimens with dimensions of  $8 \text{ mm} \times 8 \text{ mm} \times 2.5 \text{ mm}$  were cut by the electrical-discharge method. The surfaces were polished down to 800-alumina paper. The specimens were cleaned in acetone, ethanol, and distilled water in an ultrasonic bath before tests.

### 2.2. Specimen examination

The mixed  $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$  powders were prepared according to the  $\text{Na}_2\text{SO}_4$ : $\text{NaCl}$  mass ratios of 0.75:0.25, 0.35:0.65, and 0.25:0.75, respectively. In each test, one sample and mixed  $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$  salts were put into an  $\text{Al}_2\text{O}_3$  crucible, and then it was placed in an electric box furnace. The tests were conducted at  $850^\circ\text{C}$  in air. The specimens were immersed in the molten salts completely during the tests. In order to probe the influence of  $\text{NaCl}$  in the mixed salts, the corrosion behavior of  $\text{Ti}_3\text{SiC}_2$  in pure molten  $\text{NaCl}$  was also conducted at  $850^\circ\text{C}$ .

After hot corrosion tests, the samples were washed with boiling distilled water to dissolve the remains of  $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$  and other dissolvable salts, then the samples were dried in hot air. Each sample was weighted before and after the test (the sensitivity of the balance used was  $10^{-5} \text{ g}$ ). The microstructure analysis of corroded specimens was carried out by using a scanning electron microscope (SEM) equipped with an energy dispersive spectroscopy (EDS). The phase compositions of the corrosion layer were determined by X-ray diffraction (XRD).

## 3. Results and discussion

### 3.1. Kinetics of hot corrosion

Fig. 1 shows the mass change per unit area of  $\text{Ti}_3\text{SiC}_2$  as a function of time during the hot corrosion in the mixture

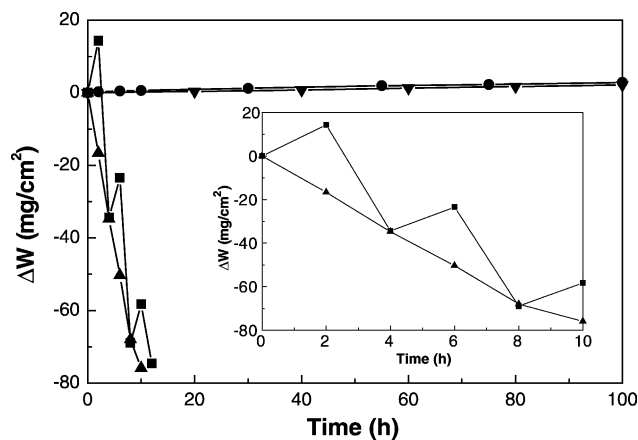


Fig. 1. The mass change per unit area as a function of time for hot corrosion of  $\text{Ti}_3\text{SiC}_2$  in the mixture of  $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$  and  $\text{NaCl}$  melts at  $850^\circ\text{C}$ . (▲) 75 wt.%  $\text{Na}_2\text{SO}_4$  + 25 wt.%  $\text{NaCl}$ ; (■) 35 wt.%  $\text{Na}_2\text{SO}_4$  + 65 wt.%  $\text{NaCl}$ ; (●) 25 wt.%  $\text{Na}_2\text{SO}_4$  + 75 wt.%  $\text{NaCl}$ ; (▼)  $\text{NaCl}$ .

of  $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$  melts and pure molten  $\text{NaCl}$  at  $850^\circ\text{C}$ . When specimen corroded in 75 wt.%  $\text{Na}_2\text{SO}_4$  + 25 wt.%  $\text{NaCl}$  mixture for 8 h, the mass change per unit area ( $\Delta W$ ) decreased monotonically. The final mass loss was about  $70 \text{ mg cm}^{-2}$  after 8 h. The results revealed that severe hot corrosion occurred during the test. When the specimen corroded in the mixture of 35 wt.%  $\text{Na}_2\text{SO}_4$  + 65 wt.%  $\text{NaCl}$  melts, although the mass loss and mass gain occurred alternately, the mass loss per unit area was observed as a whole. The final mass loss was about  $70 \text{ mg cm}^{-2}$ .

On contrary to above mentioned, obvious mass loss, it is surprising that monotonous and slight mass gain (about  $2 \text{ mg cm}^{-2}$ ) was observed when the specimens corroded in both mixture of 25 wt.%  $\text{Na}_2\text{SO}_4$  + 75 wt.%  $\text{NaCl}$  melts and pure  $\text{NaCl}$  melt even for 100 h. It suggested that the corrosion products did not spall from specimens on a large scale during the hot corrosion. Therefore, it could be concluded at this point that  $\text{Ti}_3\text{SiC}_2$  suffered disastrous hot corrosion in the mixture of  $\text{Na}_2\text{SO}_4$  +  $\text{NaCl}$  melts when the concentration of  $\text{Na}_2\text{SO}_4$  was higher than 35 wt.%.

### 3.2. Phase composition and microstructure of the corrosion products

Fig. 2a shows the surface morphology of  $\text{Ti}_3\text{SiC}_2$  after hot corrosion in the mixture of 75 wt.%  $\text{Na}_2\text{SO}_4$ –25 wt.%  $\text{NaCl}$  melts for 8 h at  $850^\circ\text{C}$ . The corrosion products spalled off on a large scale from the sample surface. Therefore, the surface morphology was differentiated into two typical regions: P is the bottom surface from which the corrosion products spalled off, T is the original surface of the outer corrosion scale, where the corrosion products did not spall off. Fig. 2b and c show higher magnification of region T and P, respectively. The corresponding EDS X-ray spectra were also included in both figures. In order to probe the phase compositions of two different regions, the outer layer corro-

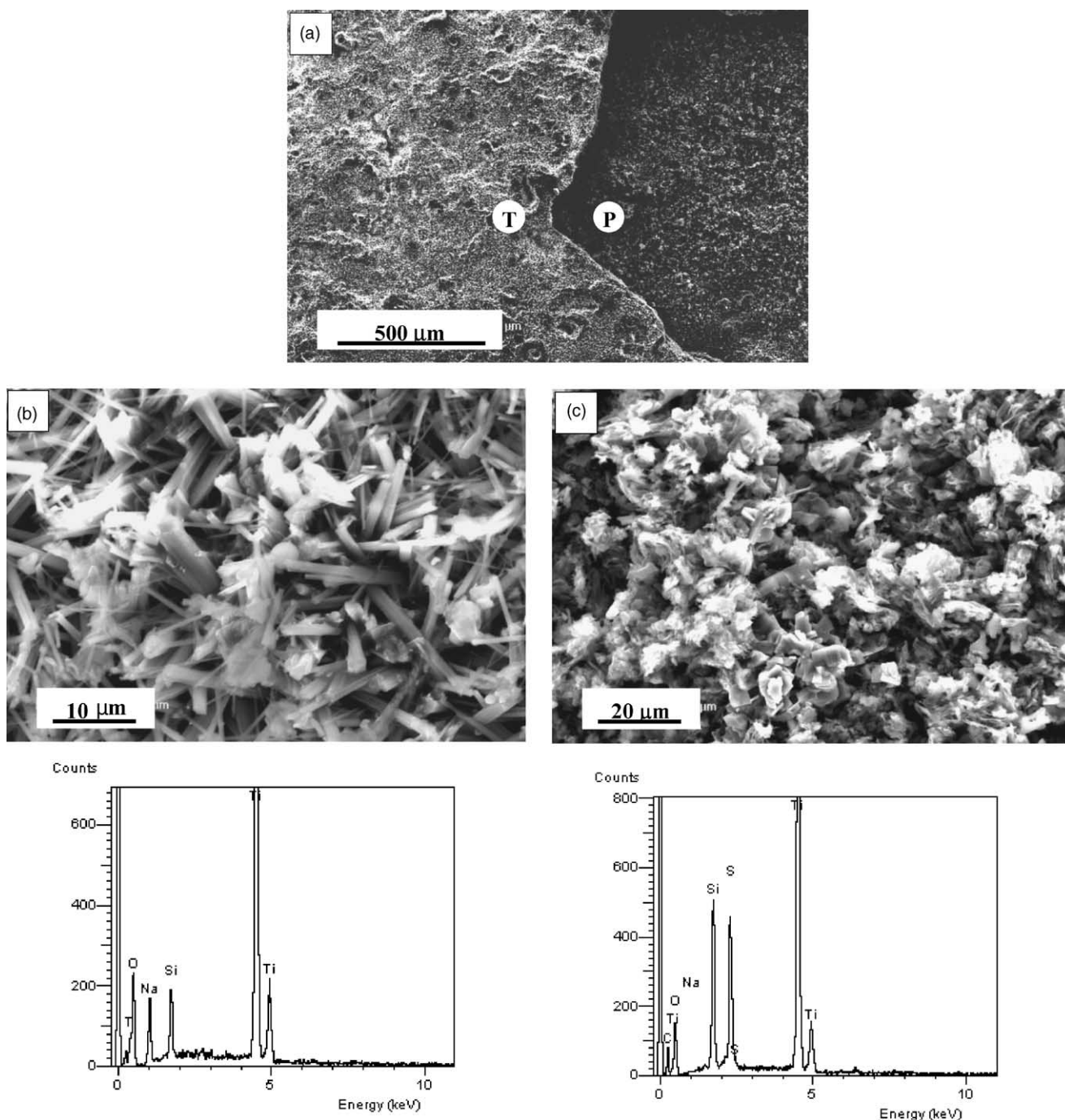


Fig. 2. The surface morphologies and corresponding EDS X-ray spectra of  $\text{Ti}_3\text{SiC}_2$  after hot corrosion in the mixture of 75 wt.%  $\text{Na}_2\text{SO}_4$ –25 wt.%  $\text{NaCl}$  melts for 8 h at  $850^\circ\text{C}$ . (a) Overview; (b) higher magnification of region T; (c) higher magnification of region P.

sion products were peeled off completely, and collected, and then the phase compositions of two regions (region T and region P) could be identified by XRD. Fig. 3 shows XRD patterns of the region T and P. It is seen from Fig. 2b that the surface of the region T consists of a number of circular crystallites. EDS analysis demonstrated that the elements in this region were consisted of Ti, O, Si, and Na. Combining the results of XRD and EDS, the main phases in this region were recognized as  $\text{Na}_{0.23}\text{TiO}_2$ ,  $\text{Na}_2\text{Ti}_6\text{O}_{13}$ ,  $\text{TiO}_2$  and

a small amount of  $\text{Na}_2\text{SiO}_3$ . In Fig. 2c, irregular protrusions formed in region P, which morphology is different from the region T. In region P,  $\text{TiO}_2$  and sulfur were identified as the main phases by XRD and EDS.

Fig. 4a and b are cross-sections of the sample corroded in the mixture of 75 wt.%  $\text{Na}_2\text{SO}_4$  + 25 wt.%  $\text{NaCl}$  melts. SEM observation revealed that the cross-sections had a two-layer microstructure. Many micro-pores were observed in the outer layer. Some radial and transverse cracks ex-



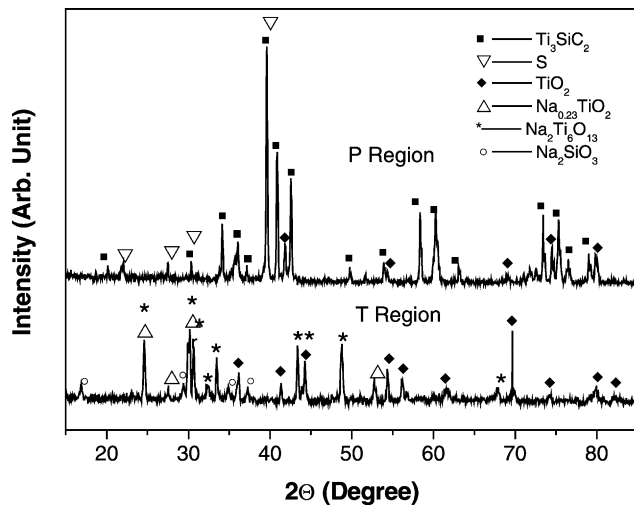


Fig. 3. XRD patterns of region P and region T.

isted in the outer and inner layer, respectively. Because two types of crack co-existed in the outer and inner corrosion layer, furthermore, sulfur segregated in the inner layer and resulted in weak bonding between the inner layer and outer

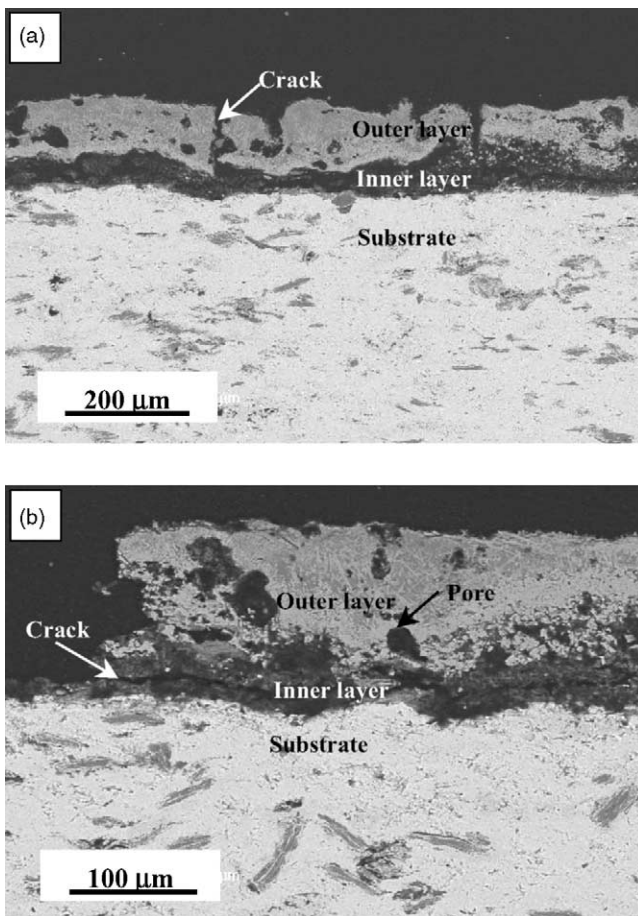


Fig. 4. The cross-sections of specimen corroded in the mixture of 75 wt.%  $\text{Na}_2\text{SO}_4$ –25 wt.%  $\text{NaCl}$  melts at  $850^\circ\text{C}$  for 8 h. (a) Overview; (b) higher magnification.

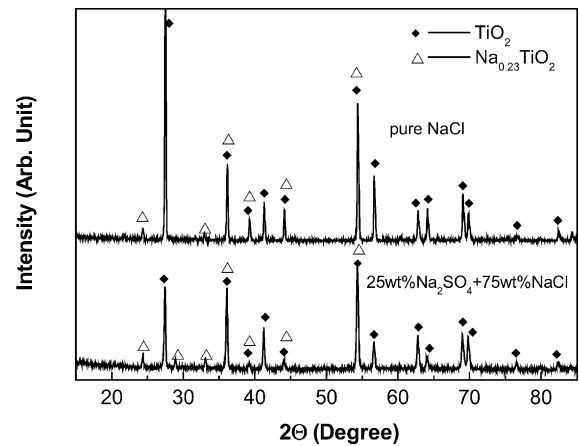


Fig. 5. XRD patterns of specimens corroded in the mixture of 25 wt.%  $\text{Na}_2\text{SO}_4$ –75 wt.%  $\text{NaCl}$  melts and  $\text{NaCl}$  melt at  $850^\circ\text{C}$  for 100 h.

layer, the outer layer spalled off easily during hot corrosion and subsequent treatments. The other mechanism for the spallation of corrosion products from substrate might be related to the  $\text{Na}^+$  presented in the mixed molten salts. It is reported that  $\text{Na}^+$  could induce devitrification in amorphous  $\text{SiO}_2$ .<sup>13</sup> The resultant volume change could lead to cracking and a breakdown of the protective  $\text{SiO}_2$  layer. Thus, even acidic salts might lead to degradation of  $\text{SiO}_2$ -protected ceramics via this mechanism. Because corrosion products spalled from specimens on a large scale, protective corrosion products could not form on the substrate, severe hot corrosion would sustain.

Fig. 5 shows the X-ray diffraction patterns of the corroded sample in the mixture of 25 wt.%  $\text{Na}_2\text{SO}_4$  + 75 wt.%  $\text{NaCl}$  melts. The main phases of corrosion products were identified as  $\text{TiO}_2$  and  $\text{Na}_{0.23}\text{TiO}_2$ . Fig. 6a and b are surface morphology and cross-section of specimen corroded in the mixture of 25 wt.%  $\text{Na}_2\text{SO}_4$  + 75 wt.%  $\text{NaCl}$  melts, respectively. Although in Fig. 6a some cracks were observed on the surface of corrosion layer, corrosion products did not spall from the specimen. The large grains on the surface were recognized as  $\text{TiO}_2$ , and the small grains were  $\text{Na}_{0.23}\text{TiO}_2$  by EDS. The cross-section of corroded samples had a duplex microstructure, i.e. an outer layer and an inner layer (divided by white mark line). In outer layer the light gray grains were recognized as  $\text{TiO}_2$ , the dark gray grains were identified as  $\text{Na}_{0.23}\text{TiO}_2$ . EDS analysis revealed that the main phases in the inner layer were  $\text{TiO}_2$  and  $\text{SiO}_2$ . The reason for the fact that no crystalline Si-containing phase was detected by XRD might be related to the following reasons. One possible reason was due to relative content of  $\text{SiO}_2$  in the corrosion products was too low to be detected. The other reason was related to the thickness of the outer layer (about  $15\ \mu\text{m}$ ), which led to characteristic peaks of Si-containing phase in the inner layer could not be detected by XRD. Similarly, in Fig. 6b some pores were observed in the cross-section.

Fig. 7a and b are surface morphology and cross-section of the specimen corroded in the pure  $\text{NaCl}$  melt, respectively.

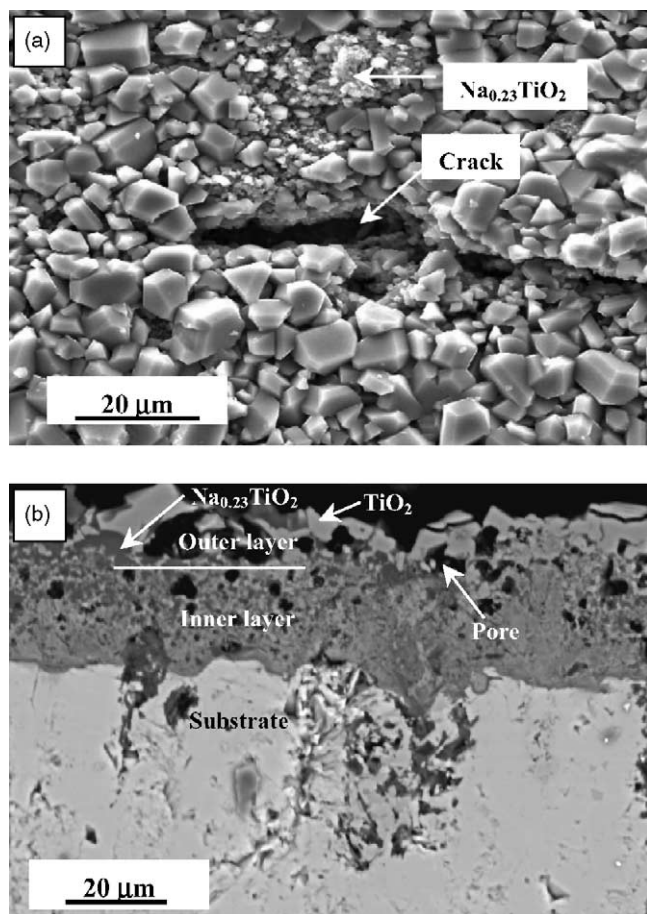
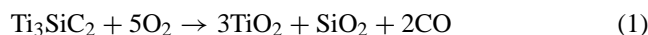


Fig. 6. Morphologies of (a) surface and (b) cross-section of specimen corroded in 25 wt.%  $\text{Na}_2\text{SO}_4$ –75 wt.%  $\text{NaCl}$  at  $850^\circ\text{C}$  for 100h.

The microstructures were very similar to those in Fig. 6a and b. However, no crack was observed on the surface of the corrosion layer; less pores existed in the cross-section, which denoted that the specimen exhibited better hot corrosion resistance in pure  $\text{NaCl}$  melt. The phase compositions were also determined to be  $\text{TiO}_2$  and  $\text{Na}_{0.23}\text{TiO}_2$  by XRD (see Fig. 5).

### 3.3. Mechanism for the corrosion of $\text{Ti}_3\text{SiC}_2$

It is reported that  $\text{Ti}_3\text{SiC}_2$  suffered severe hot corrosion in the eutectic  $\text{K}_2\text{CO}_3$  and  $\text{Li}_2\text{CO}_3$  mixture at  $850^\circ\text{C}$ .<sup>9,10</sup> It was considered that corrosion of this material in the eutectic  $\text{K}_2\text{CO}_3$ – $\text{Li}_2\text{CO}_3$  mixture was caused by the dissolution of  $\text{SiO}_2$  and  $\text{TiO}_2$ , which formed by the oxidation of  $\text{Ti}_3\text{SiC}_2$  owing to dissolved oxygen.<sup>7</sup>



The corrosion rate was related to the basicity of carbonates. However,  $\text{Na}_2\text{SO}_4$  tended to dissociate less than (Li,K)-carbonates and hence is more acidic. Shi and Rapp<sup>14</sup> measured the solubility of  $\text{SiO}_2$  in  $\text{Na}_2\text{SO}_4$  for  $a_{\text{Na}_2\text{O}}$  from  $10^{-11}$  to  $10^{-14}$  at  $900^\circ\text{C}$ . Over the range they obtained a

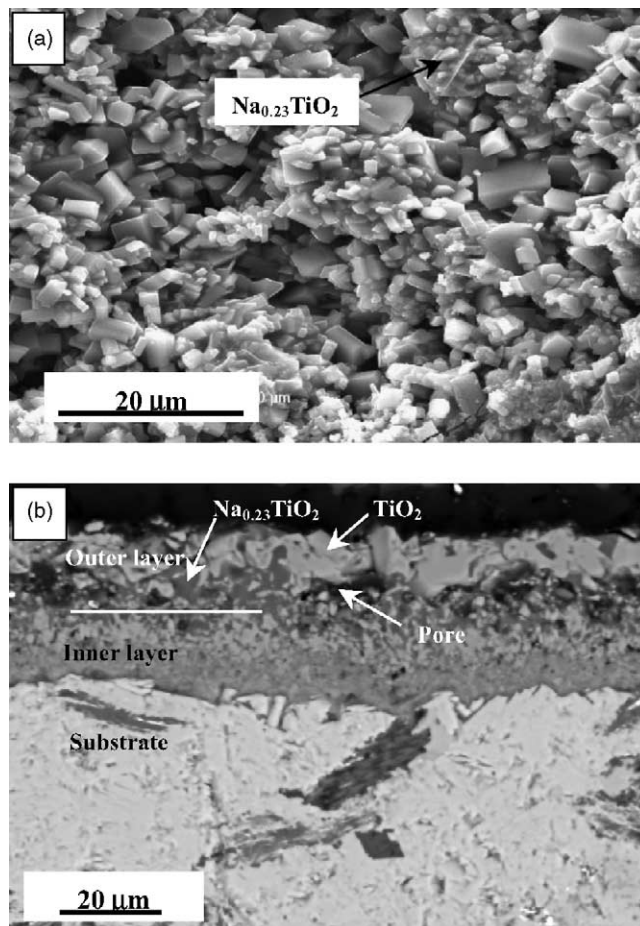
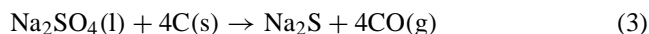
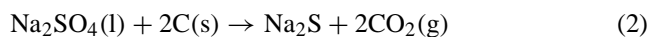


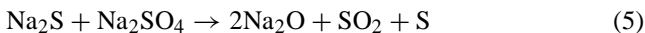
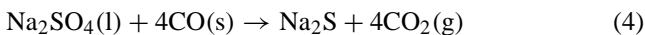
Fig. 7. Morphologies of (a) surface and (b) cross-section of specimen corroded in pure  $\text{NaCl}$  melt at  $850^\circ\text{C}$  for 100h.

very limited and constant solubility of  $3.2 \pm 1.8$  ppm by weight. However, this experimental results revealed that when the concentration of  $\text{Na}_2\text{SO}_4$  was higher than 35 wt.%, the corrosion rate of  $\text{Ti}_3\text{SiC}_2$  in molten  $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$  salts at  $850^\circ\text{C}$  was very fast (the average mass loss rate was about  $8.75 \text{ mg cm}^{-2} \text{ h}^{-1}$  in 8 h), which was higher than that of  $\text{Ti}_3\text{SiC}_2$  corroded in the mixture of (Li,K) $_2\text{CO}_3$  melts at  $850^\circ\text{C}$  (the average mass loss rate was about  $3.75 \text{ mg cm}^{-2} \text{ h}^{-1}$  in 8 h).<sup>10</sup> The reason for this was thought to be related to C existing in  $\text{Ti}_3\text{SiC}_2$ . C and CO could act as a reducing agent at high-temperature. It is reported that the addition of carbon to pure sodium sulfate led to the formation of  $\text{CO}_2$  or CO, which made the following process favorable:<sup>15</sup>

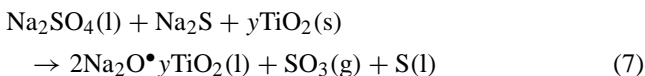
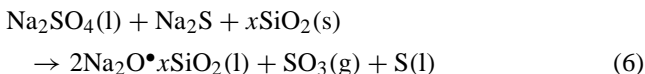


The formation of  $\text{Na}_2\text{S}$  has been observed experimentally in a pure  $\text{Na}_2\text{SO}_4 + \text{C}$  system.<sup>15</sup> According to the above reactions, we could conclude that the released CO from the oxidation of  $\text{Ti}_3\text{SiC}_2$  might be sufficient to create basic con-

ditions:

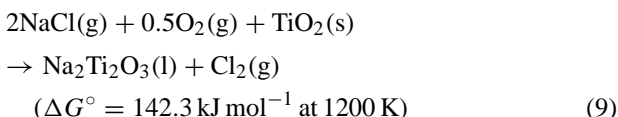
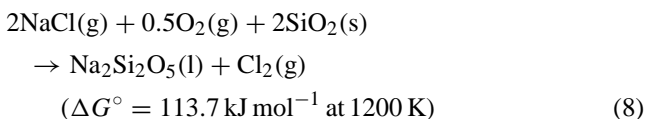


$\text{Na}_2\text{SO}_4$  and  $\text{Na}_2\text{S}$  could form a eutectic melts with a melting temperature of about 740 °C and react with the newly formed  $\text{SiO}_2$  and  $\text{TiO}_2$  according to the following reactions:<sup>16</sup>



where  $x$  and  $y$  were variable coefficients. Therefore, when the concentration of  $\text{Na}_2\text{SO}_4$  was higher than 35 wt.%, the corrosion rate of  $\text{Ti}_3\text{SiC}_2$  in  $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$  melts was very high. On the other hand, because the melting point of  $\text{NaCl}$  (801 °C) was lower than that of  $\text{Na}_2\text{SO}_4$  (884 °C), the mixed salts melted and liquid corrodent covered the samples at 850 °C, which would lead to faster corrosion rate. According to reactions (6) and (7), when  $\text{Na}_2\text{SO}_4$  and  $\text{Na}_2\text{S}$  penetrated the out layer and corrosion occurred at the interface of corrosion layer and substrate, sulfur would segregated in the inner layer. This was the reason why sulfur was detected in the inner corrosion layer. Sulfur segregated in the inner layer resulted in corrosion products spall off easily, corrosion products could not protect substrate, and then corrosion of sample was accelerated.

It is reported that some alloys such as Ti–50Al, Ti–50Al–10Cr exhibited good hot corrosion resistance in  $\text{Na}_2\text{SO}_4$  melt at 900 °C, however, these alloys suffered severe hot corrosion attack in  $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$  melts at 850 °C.<sup>17</sup> As mentioned previously,  $\text{Ti}_3\text{SiC}_2$  exhibited excellent corrosion resistance in pure  $\text{NaCl}$  melt. The main reason might be related to stable protective oxide film formed on the specimen surface in  $\text{NaCl}$  melt. During the initial corrosion stage,  $\text{Ti}_3\text{SiC}_2$  was oxidized by the dissolved oxygen in the  $\text{NaCl}$  melt according to reaction (1). Oxygen diffused through the molten salts to specimens and reacted with  $\text{NaCl}$  and newly formed  $\text{TiO}_2$  and  $\text{SiO}_2$ . Some investigators proposed reactions as follows:<sup>18,19</sup>



However, both reactions (8) and (9) are not thermodynamically favored. Considering most oxygen dissolved in melts was consumed by reaction (1) and resulted in very low oxygen partial pressure in the melts, which was also adverse to

reactions (8) and (9). Therefore,  $\text{Ti}_3\text{SiC}_2$  exhibited excellent corrosion resistance in the molten  $\text{NaCl}$ .

As mentioned in the above sections, before hot corrosion occurred,  $\text{Ti}_3\text{SiC}_2$  was oxidized first to form  $\text{TiO}_2$  and  $\text{SiO}_2$ .  $\text{SiO}_2$  played a crucial role for oxidation resistance. The reaction process could be modeled with rate control by an interfacial solution of  $\text{SiO}_2$  and  $\text{TiO}_2$  into the melts at a rate proportional to the instantaneous melt composition.<sup>20</sup> When the specimens corroded in the mixture of 25 wt.%  $\text{Na}_2\text{SO}_4$  + 75 wt.%  $\text{NaCl}$  melts, the mixture of melts could not create sufficient basicity ( $a_{\text{Na}_2\text{O}}$ ). The oxidation rate of  $\text{Ti}_3\text{SiC}_2$  was higher than the reaction rate of oxides ( $\text{TiO}_2$  and  $\text{SiO}_2$ ) with the mixture of melts. Therefore, the protective mixture of oxide layer ( $\text{SiO}_2$  +  $\text{TiO}_2$ ) formed on the specimen surface. Actually, the mixed oxide layer was observed in Figs. 6b and 7b. Once the protective oxide layer formed on the substrate, the hot corrosion rate of specimens would decrease dramatically. This was the main reason why corrosion rate was very slow in the mixture of 25 wt.%  $\text{Na}_2\text{SO}_4$  + 75 wt.%  $\text{NaCl}$  melts.

As described above, many pores existed in each cross-sections of corrosion layer. According to reactions (1)–(5),  $\text{CO}$ ,  $\text{CO}_2$ , and  $\text{SO}_2$  would generate during oxidation and hot corrosion. These gases diffused outward from substrate through melts. Parts of bubbles released from the molten salts, however, parts of bubbles trapped in the final corrosion product, thus the pores in the corrosion layer formed. Similar phenomenon was observed when  $\alpha$ - $\text{SiC}$  was corroded at 1000 °C by  $\text{Na}_2\text{SO}_4$ .<sup>15</sup>

#### 4. Conclusions

$\text{Ti}_3\text{SiC}_2$  suffered severe hot corrosion attack in the mixture of  $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$  melts when the concentration of  $\text{Na}_2\text{SO}_4$  was higher than 35 wt.% at 850 °C. The corrosion layer had duplex microstructure; some radial and transverse cracks existed in the outer and inner layer, respectively. The corrosion products tended to spall from substrate.  $\text{C}$  and  $\text{CO}$  acted as reducing agents at high-temperature and increased the basicity of melts greatly and resulted in high corrosion rate. The presence of  $\text{NaCl}$  accelerated the corrosion rate for its lower melting point in the mixture of  $\text{Na}_2\text{SO}_4$ – $\text{NaCl}$  melts. When the concentration of  $\text{Na}_2\text{SO}_4$  was lower than 25 wt.% corrosion rate of  $\text{Ti}_3\text{SiC}_2$  was quite slow and the corrosion products did not spall at 850 °C. Because of low basicity in the mixture of melts, the protective oxide layer of  $\text{TiO}_2$  +  $\text{SiO}_2$  formed and led to low corrosion rate of  $\text{Ti}_3\text{SiC}_2$ .

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